

# Modele złożone

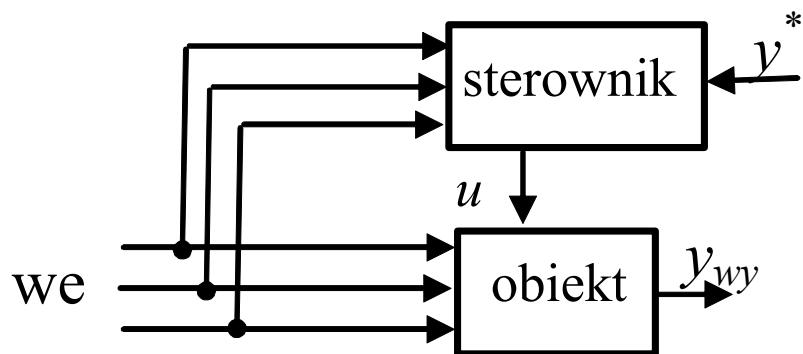
Rozbudowa modelu

- układy sterowania (regulacji)
- modele obiektów (procesów) technologicznych

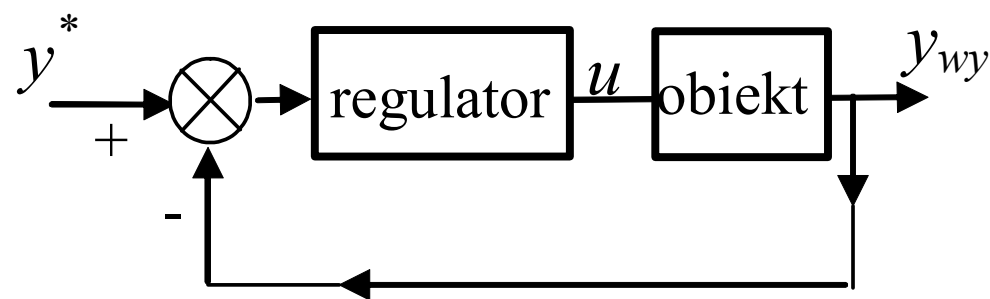
# Sterowanie w

układzie otwartym

układzie zamkniętym  
(regulacja)

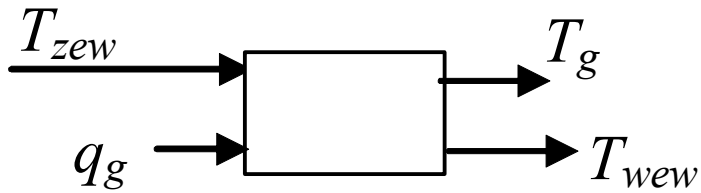


- znany „przepis” na sterowanie
- stabilne
- niedokładne



- sterowanie jest wypracowywane
- stabilne/niestabilne
- dokładne

# Regulator ciągły PI

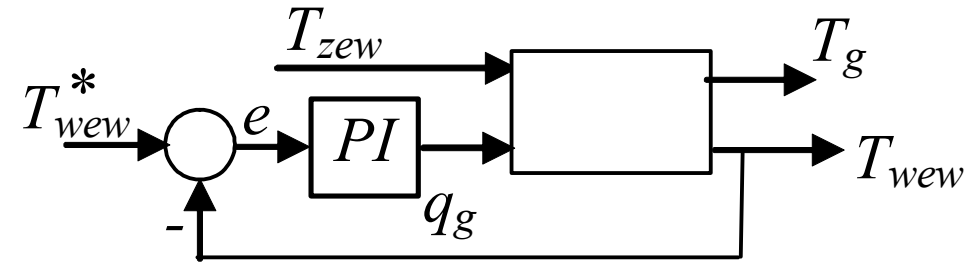
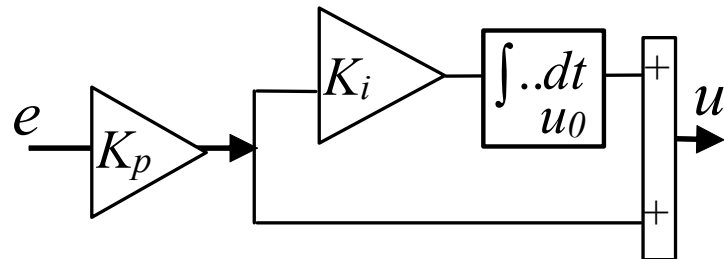


$$\begin{cases} 0 = K_{cg}(T_g - T_{wew}) - K_{cw}(T_{wew} - T_{zew}) \\ 0 = q_g - K_{cg}(T_g - T_{wew}) \end{cases}$$

wejścia:  $T_{zew0}, q_{g0}$

$$T_{wew0} = \dots$$

$$T_{g0} = \dots$$



$$\begin{cases} 0 = K_{cg}(T_g - T_{wew}) - K_{cw}(T_{wew} - T_{zew}) \\ 0 = q_g - K_{cg}(T_g - T_{wew}) \\ T_{wew} = T_{zew}^* \end{cases}$$

wejścia:  $T_{zew0}, T_{zew0}^*, e = 0$

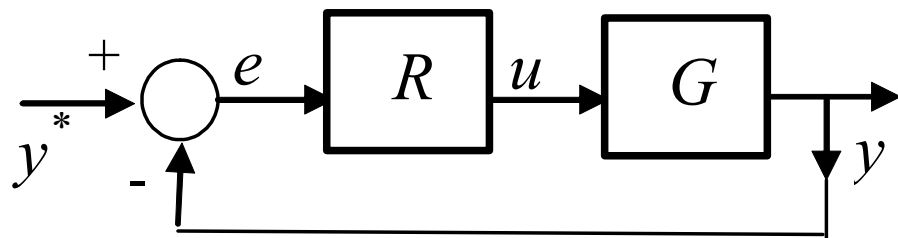
$$q_{g0} = \dots$$

$$T_{wew0} = T_{zew0}^*$$

$$T_{g0} = \dots$$

$$PI: R = K_p \left( 1 + \frac{1}{T_i s} \right)$$

# Transmitancje układu regulacji ciągłej



$$\begin{cases} Y(s) = G(s)U(s) \\ U(s) = R(s)E(s) \\ E(s) = Y^*(s) - Y(s) \end{cases}$$

$$\frac{Y}{Y^*} = G_z = \frac{RG}{1 + RG} \quad \text{t.układu zamkniętego}$$

$$Y(s) = \frac{R(s)G(s)}{1 + R(s)G(s)} Y^*(s)$$

$$\frac{E}{Y^*} = G_e = \frac{1}{1 + RG} \quad \text{t.uchybowa}$$

$$E(s) = \frac{1}{1 + R(s)G(s)} Y^*(s)$$

$$G(s) = \frac{L_o(s)}{M_o(s)}$$

$$G_z = \frac{L_o(s)L_R(s)}{M_o(s)M_R(s) + L_o(s)L_R(s)}$$

$$R(s) = \frac{L_R(s)}{M_R(s)}$$

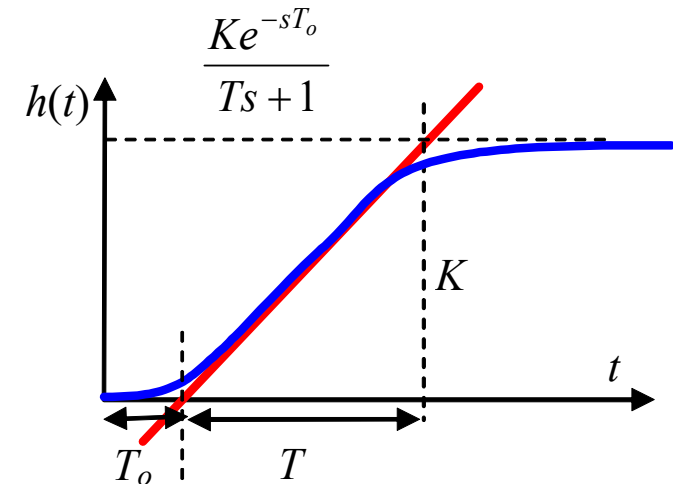
$$G_e = \frac{M_o(s)M_R(s)}{M_o(s)M_R(s) + L_o(s)L_R(s)}$$

# Dobór nastaw PID (auto-tuning, samonastrajanie)

## ► Metoda Zieglera-Nicholsa (odpowiedzi skokowej)

- identyfikacja modelu (przy otwartej pętli)
- nastawy wg tabel dla różnych klas obiektów

Regulator	$K_p$	$T_i$	$T_d$
<b>PI</b>	$\frac{0,9T}{KT_o}$	$3,33T_o$	
<b>PID</b>	$\frac{1,2T}{KT_o}$	$2T_o$	$0,5T_o$

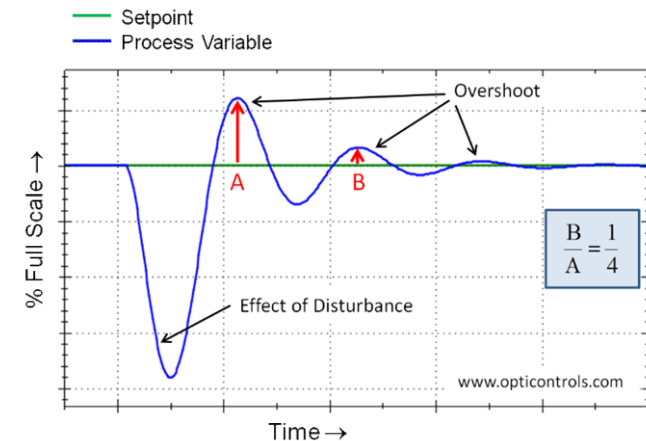


## Metoda QDR (Quarter-Decay Ratio)

- każde następne przeregulowanie ma amplitudę 4 razy mniejszą od poprzedniej

### Uwagi:

- Esperyment Zieglera-Nicholsa (1942) zautomatyzowany w latach '70
- (+) prosty eksperyment
- (-) identyfikacja modelu obiektu przy rozwartej pętli regulacji
- **PID-kaskadowy (interacting)**
- A jeśli  $T_o \approx 0$ ?



## Praktyka inżynierska – korzystamy z tego co mamy

Urządzenia realizujące regulację:

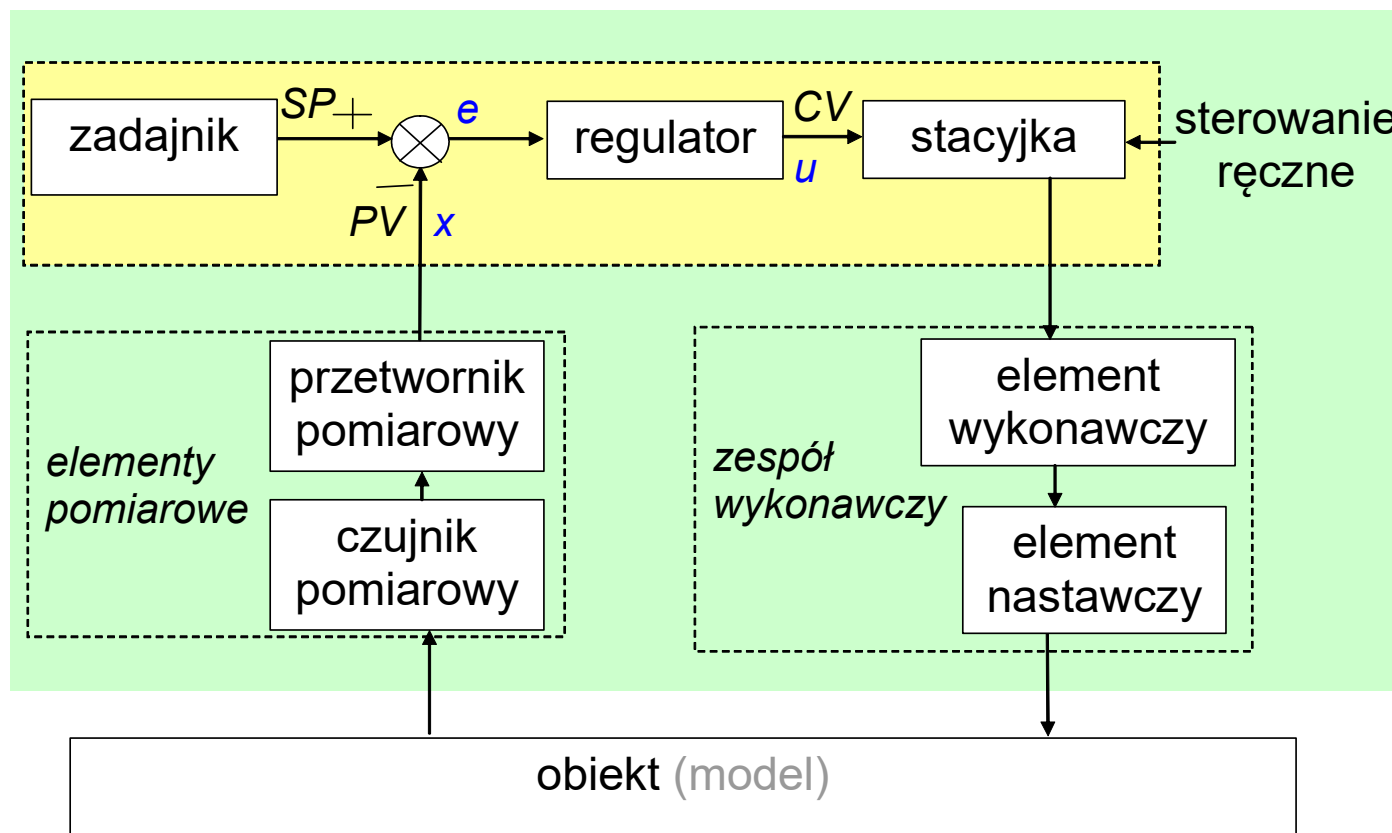
- blok funkcyjny PID w sterowniku PLC
- moduł PID w sterowniku PLC
- regulator wielofunkcyjny
- prosty regulator cyfrowy



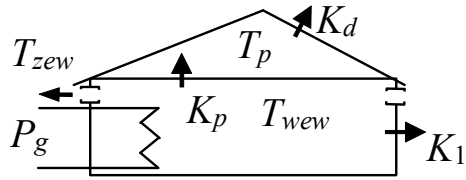
## Praktyka inżynierska - regulatory

Urządzenia automatyki:

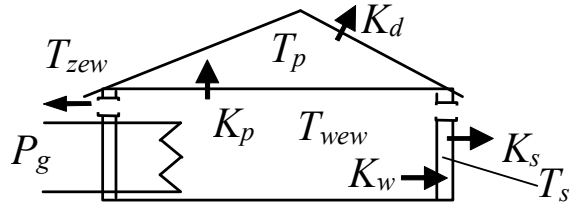
- elementy pomiarowe
- elementy wykonawcze
- sterowniki, regulator



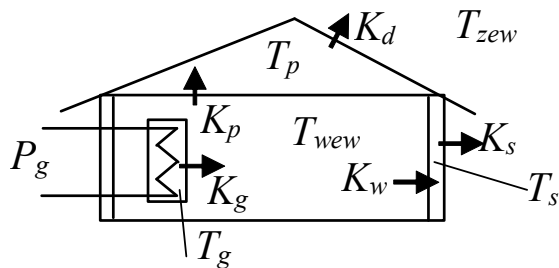
# Rozbudowa modelu



$$\begin{cases} C_{vw} \dot{T}_{wew}(t) = P_g(t) - K_1(T_{wew}(t) - T_{zew}(t)) - K_p(T_{wew}(t) - T_p(t)) - c_p \rho_p f_p(t)(T_{wew}(t) - T_{zew}(t)) \\ C_{vp} \dot{T}_p(t) = K_p(T_{wew}(t) - T_p(t)) - K_d(T_p(t) - T_{zew}(t)) \end{cases}$$



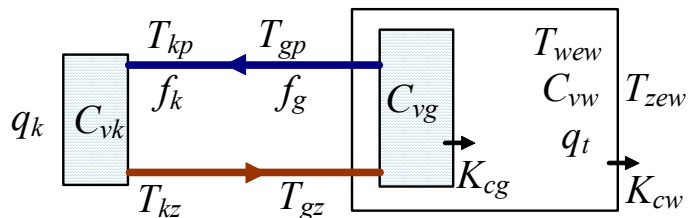
$$\begin{cases} C_{vw} \dot{T}_{wew}(t) = P_g(t) - K_w(T_{wew}(t) - T_s(t)) - K_p(T_{wew}(t) - T_p(t)) - c_p \rho_p f_p(t)(T_{wew}(t) - T_{zew}(t)) \\ C_{vs} \dot{T}_s(t) = K_w(T_{wew}(t) - T_s(t)) - K_s(T_s(t) - T_{zew}(t)) \\ C_{vp} \dot{T}_p(t) = K_p(T_{wew}(t) - T_p(t)) - K_d(T_p(t) - T_{zew}(t)) \end{cases}$$



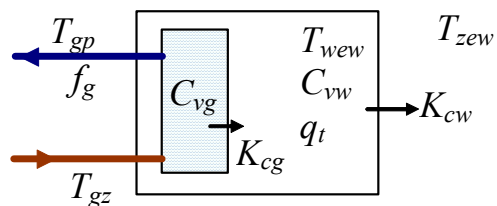
$$\begin{cases} C_{vg} \dot{T}_g(t) = P_g(t) - K_g(T_g(t) - T_{wew}(t)) \\ C_{vw} \dot{T}_{wew}(t) = K_g(T_g(t) - T_{wew}(t)) - K_w(T_{wew}(t) - T_s(t)) - K_p(T_{wew}(t) - T_p(t)) \\ C_{vs} \dot{T}_s(t) = K_w(T_{wew}(t) - T_s(t)) - K_s(T_s(t) - T_{zew}(t)) \\ C_{vp} \dot{T}_p(t) = K_p(T_{wew}(t) - T_p(t)) - K_d(T_p(t) - T_{zew}(t)) \end{cases}$$



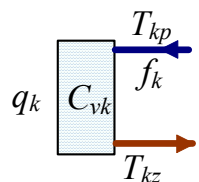
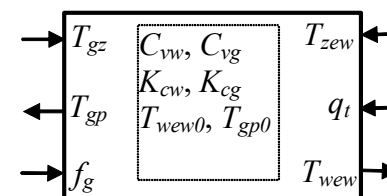
# Własna biblioteka modeli



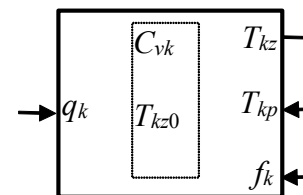
Blok (subsystem)



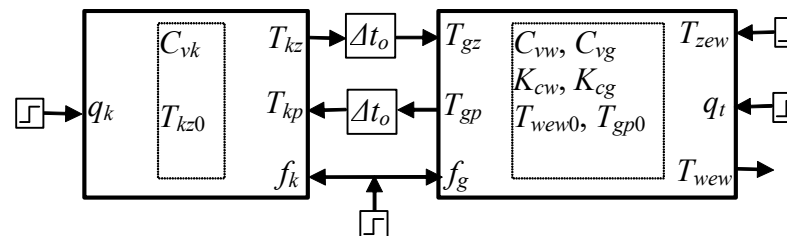
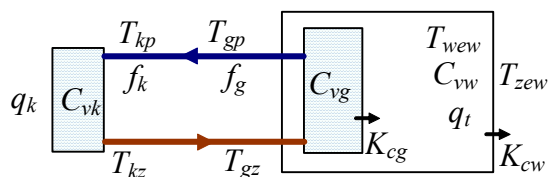
$$\begin{cases} C_{vw} \dot{T}_{wew} = K_{cg} (T_{gp} - T_{wew}) - K_{cw} (T_{wew} - T_{zew}) + q_t \\ C_{vg} \dot{T}_{gp} = c_{pw} f_{mg} (T_{gz} - T_{gp}) - K_{cg} (T_{gp} - T_{wew}) \end{cases}$$



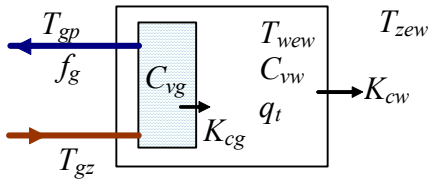
$$C_{vk} \dot{T}_{kz} = q_k - c_{pw} f_{mk} (T_{kz} - T_{kp})$$



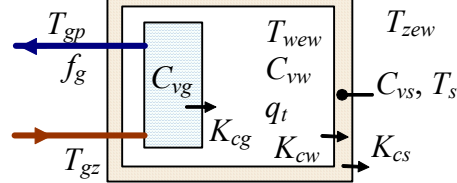
Schemat oparty na blokach



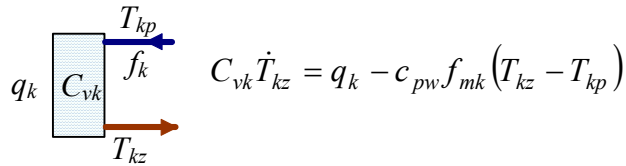
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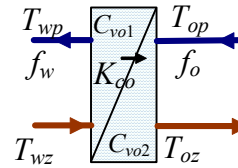
$$\begin{cases} C_{vw} \dot{T}_{wew} = K_{cg}(T_{gp} - T_{wew}) - K_{cw}(T_{wew} - T_{zew}) + q_t \\ C_{vg} \dot{T}_{gp} = c_{pw} f_{mg}(T_{gz} - T_{gp}) - K_{cg}(T_{gp} - T_{wew}) \end{cases}$$



$$\begin{cases} C_{vw} \dot{T}_{wew} = K_{cg}(T_{gp} - T_{wew}) - K_{cw}(T_{wew} - T_s) + q_t \\ C_{vg} \dot{T}_{gp} = c_{pw} f_{mg}(T_{gz} - T_{gp}) - K_{cg}(T_{gp} - T_{wew}) \\ C_{vs} \dot{T}_s = K_{cw}(T_{wew} - T_s) - K_{cs}(T_s - T_{zew}) \end{cases}$$



$$C_{vk} \dot{T}_{kz} = q_k - c_{pw} f_{mk}(T_{kz} - T_{kp})$$



$$\begin{cases} C_{vo2} \dot{T}_{oz} = K_{co}(T_{wp} - T_{oz}) - c_{pw} f_{mo}(T_{oz} - T_{op}) \\ C_{vo1} \dot{T}_{wp} = c_{pw} f_{mw}(T_{wz} - T_{wp}) - K_{co}(T_{wp} - T_{oz}) \end{cases}$$

