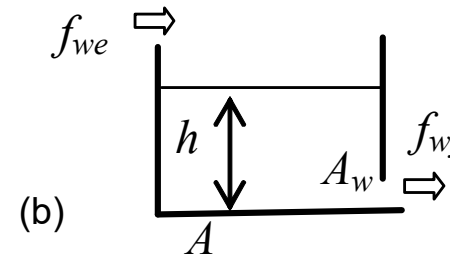
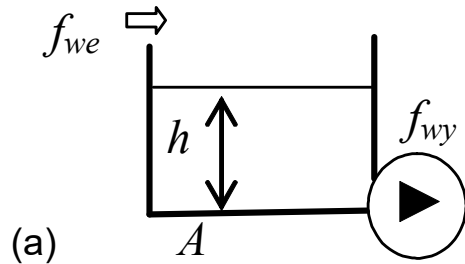


## Otwarte układy hydrauliczne – zasada konstrukcji modelu



1) Zawartość magazynu

$$V(t) = Ah(t) \quad [m^2 \cdot m = m^3]$$

2) Zmiana zawartości magazynu

$$\frac{dV(t)}{dt} = A \frac{dh(t)}{dt} = A\dot{h}(t) \quad \left[ m^2 \cdot \frac{m}{s} = \frac{m^3}{s} \right]$$

3) Bilans strumieni wpływających i wypływających [m<sup>3</sup>/s]

$$A\dot{h}(t) = f_{we}(t) - f_{wy}(t)$$

(a)  $f_{wy}(t)$

(b)  $f_{wy}(t) = A_w \sqrt{2gh(t)} \approx ah(t)$

(a)  $A\dot{h}(t) = f_{we}(t) - f_{wy}(t)$

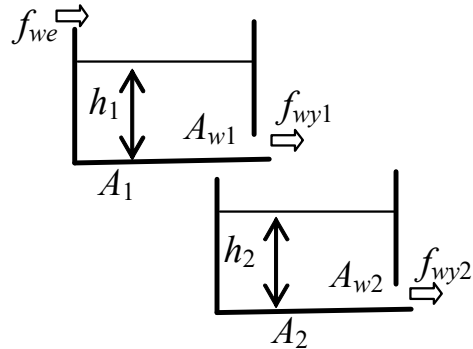
(b<sub>1</sub>)  $A\dot{h}(t) = f_{we}(t) - A_w \sqrt{2gh(t)}$

(b<sub>2</sub>)  $A\dot{h}(t) = f_{we}(t) - ah(t)$

4) Zmienne wejściowe i wyjściowe, kompletność modelu

5) Identyfikacja wartości parametrów

# Otwarte układy hydrauliczne



$$\begin{cases} A_1 \dot{h}_1(t) = f_{we}(t) - f_{wy1}(t) \\ A_2 \dot{h}_2(t) = f_{wy1}(t) - f_{wy2}(t) \\ f_{wy1}(t) = A_{w1} \sqrt{2gh_1(t)} \approx a_1 h_1(t) \\ f_{wy2}(t) = A_{w2} \sqrt{2gh_2(t)} \approx a_2 h_2(t) \end{cases}$$

$$\begin{cases} A_1 \dot{h}_1(t) = f_{we}(t) - A_{w1} \sqrt{2gh_1(t)} \\ A_2 \dot{h}_2(t) = A_{w1} \sqrt{2gh_1(t)} - A_{w2} \sqrt{2gh_2(t)} \end{cases}$$

$$\begin{cases} A_1 \dot{h}_1(t) = f_{we}(t) - a_1 h_1(t) \\ A_2 \dot{h}_2(t) = a_1 h_1(t) - a_2 h_2(t) \end{cases}$$

Równania dynamiki

$$\begin{cases} 0 = f_{we} - A_{w1} \sqrt{2gh_1} \\ 0 = A_{w1} \sqrt{2gh_1} - A_{w2} \sqrt{2gh_2} \end{cases}$$

$$\begin{cases} 0 = f_{we} - a_1 h_1 \\ 0 = a_1 h_1 - a_2 h_2 \end{cases}$$

Równania statyczne

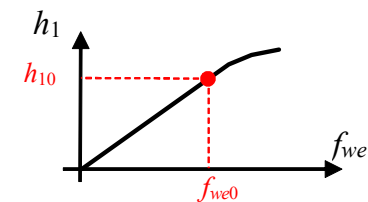
$$\Rightarrow h_1 = \frac{f_{we}^2}{2gA_{w1}^2} \quad h_2 = \frac{f_{we}^2}{2gA_{w2}^2}$$

$$\Rightarrow h_1 = \frac{f_{we}}{a_1} \quad h_2 = \frac{f_{we}}{a_2}$$

Charakterystyki statyczne

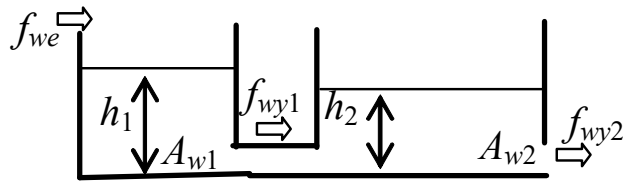
Punkt równowagi

Punkt pracy



Identyfikacja parametrów ( $A_1, A_2, A_{w1}, A_{w2}$ )

## Otwarte układy hydrauliczne



$$\begin{cases} A_1 \dot{h}_1(t) = f_{we}(t) - f_{wy1}(t) \\ A_2 \dot{h}_2(t) = f_{wy1}(t) - f_{wy2}(t) \end{cases}$$

$$f_{wy1}(t) = A_{w1} \sqrt{2g(h_1(t) - h_2(t))} \approx a_1(h_1(t) - h_2(t))$$

$$f_{wy2}(t) = A_{w2} \sqrt{2gh_2(t)} \approx a_2 h_2(t)$$

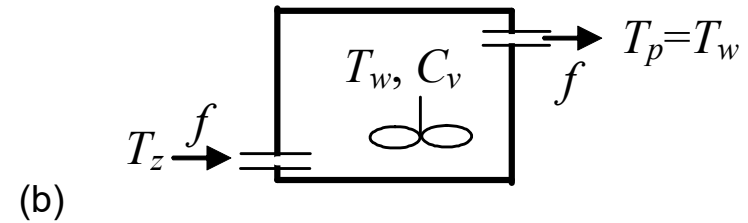
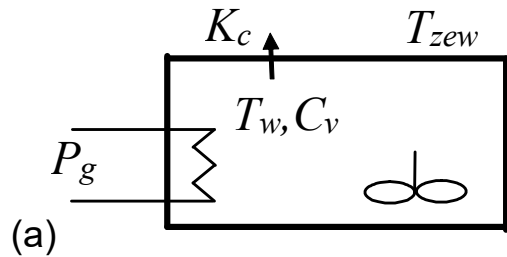
$$\begin{cases} A_1 \dot{h}_1(t) = f_{we}(t) - A_{w1} \sqrt{2g(h_1(t) - h_2(t))} \\ A_2 \dot{h}_2(t) = A_{w1} \sqrt{2g(h_1(t) - h_2(t))} - A_{w2} \sqrt{2gh_2(t)} \end{cases}$$

$$\begin{cases} 0 = f_{we} - A_{w1} \sqrt{2g(h_1 - h_2)} \\ 0 = A_{w1} \sqrt{2g(h_1 - h_2)} - A_{w2} \sqrt{2gh_2} \end{cases} \Rightarrow h_1 = \dots \quad h_2 = \dots$$

$$\begin{cases} A_1 \dot{h}_1(t) = f_{we}(t) - a_1(h_1(t) - h_2(t)) \\ A_2 \dot{h}_2(t) = a_1(h_1(t) - h_2(t)) - a_2 h_2(t) \end{cases}$$

$$\begin{cases} 0 = f_{we} - a_1(h_1 - h_2) \\ 0 = a_1(h_1 - h_2) - a_2 h_2 \end{cases} \Rightarrow h_1 = \dots \quad h_2 = \dots$$

## Obiekty cieplne – zasada konstrukcji modelu



Założenie o doskonałym mieszaniu

1) Zawartość magazynu

$$Q(t) = c_p \rho V T(t) = C_V T(t)$$

$$\left[ \frac{J}{kgK} \frac{kg}{m^3} m^3 K = \frac{J}{K} \cdot K = J \right]$$

2) Zmiana zawartości magazynu

$$\frac{dQ(t)}{dt} = C_V \frac{dT_w(t)}{dt} = C_V \dot{T}_w(t)$$

$$\left[ \frac{J}{K} \cdot \frac{K}{s} = \frac{J}{s} = \frac{Ws}{s} = W \right]$$

3) Bilans strumieni wpływających i wypływających [W]

$$C_V \dot{T}_w(t) = P_{we}(t) - P_{wy}(t)$$

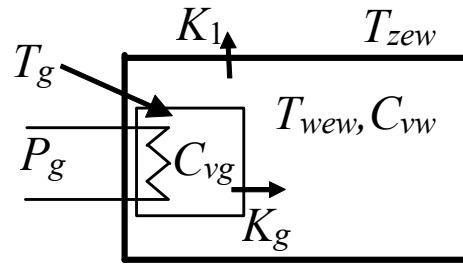
$$C_V \dot{T}_w(t) = P_g(t) - K_c (T_w(t) - T_{zew}(t))$$

$$C_V \dot{T}_w(t) = c_p \rho f(t) T_z(t) - c_p \rho f(t) T_w(t)$$

4) Zmienne wejściowe i wyjściowe, kompletność modelu

5) Identyfikacja wartości parametrów

## Obiekty cieplne



$$\begin{cases} C_{vg} \dot{T}_g(t) = P_g(t) - K_g (T_g(t) - T_{wew}(t)) \\ C_{vw} \dot{T}_{wew}(t) = K_g (T_g(t) - T_{wew}(t)) - K_1 (T_{wew}(t) - T_{zew}(t)) \end{cases}$$

wy:  $T_g, T_{wew}$

we:  $P_g, T_{zew}$

$T_g(t), T_{wew}(t)$

$P_g(t), T_{zew}(t)$

### Równania statyczne

$$\begin{cases} 0 = P_g - K_g (T_g - T_{wew}) \\ 0 = K_g (T_g - T_{wew}) - K_1 (T_{wew} - T_{zew}) \end{cases}$$

---


$$P_g = K_g (T_g - T_{wew}) = K_1 (T_{wew} - T_{zew})$$

### Obliczanie pojemności ( $C_{vg}, C_{vw}$ )

$$C_v = c_p \rho V$$

Dane:  $P_{gN}, T_{zewN}, T_{wewN}, T_{gN}$

### Identyfikacja parametrów ( $K_g, K_1$ )

$$K_1 = \frac{P_{gN}}{T_{wewN} - T_{zewN}}$$

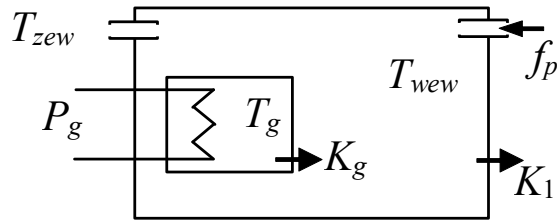
$$K_g = \frac{P_{gN}}{T_{gN} - T_{wewN}}$$

### Stan ustalony (punkt równowagi)

$$T_{wew} = \frac{P_g}{K_1} + T_{zew}$$

$$T_g = \frac{P_g}{K_g} + T_{wew} = \frac{P_g}{K_g} + \frac{P_g}{K_1} + T_{zew}$$

## Obiekty cieplne



$$\begin{cases} C_{vg} \dot{T}_g(t) = P_g(t) - K_g (T_g(t) - T_{zew}(t)) \\ C_{vw} \dot{T}_{zew}(t) = K_g (T_g(t) - T_{zew}(t)) - K_1 (T_{zew}(t) - T_{zew}(t)) + c_{pp} \rho_p f_p(t) T_{zew}(t) - c_{pp} \rho_p f_p(t) T_{zew}(t) \end{cases}$$

$$\begin{cases} C_{vg} \dot{T}_g(t) = P_g(t) - K_g (T_g(t) - T_{zew}(t)) \\ C_{vw} \dot{T}_{zew}(t) = K_g (T_g(t) - T_{zew}(t)) - K_1 (T_{zew}(t) - T_{zew}(t)) - c_{pp} \rho_p f_p(t) (T_{zew}(t) - T_{zew}(t)) \end{cases}$$

wy:  $T_g, T_{zew}$

we:  $P_g, T_{zew}, f_p$

$$\begin{cases} 0 = K_g (T_g - T_{zew}) - K_1 (T_{zew} - T_{zew}) - c_{pp} \rho_p f_p (T_{zew} - T_{zew}) \\ 0 = P_g - K_g (T_g - T_{zew}) \end{cases}$$

$$P_g = K_g (T_g - T_{zew}) = K_1 (T_{zew} - T_{zew}) + c_{pp} \rho_p f_p (T_{zew} - T_{zew})$$

$$T_{zew0} = \frac{P_{g0}}{K_1 + c_{pp} \rho_p f_{p0}} + T_{zew0}$$

$$T_{g0} = \frac{P_{g0}}{K_g} + T_{zew0} = \frac{P_{g0}}{K_g} + \frac{P_{g0}}{K_1 + c_{pp} \rho_p f_p} + T_{zew0}$$

Obliczanie pojemności ( $C_{vg}, C_{vw}$ )

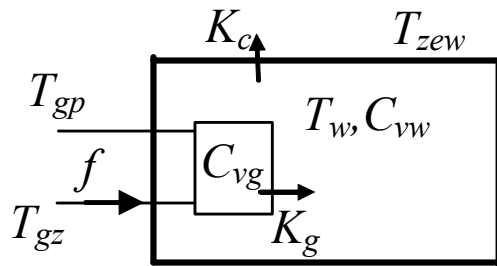
Dane:  $q_{gN}, T_{zewN}, T_{zewN}, T_{gN}$

Identyfikacja parametrów ( $K_g, K_1$ )

1)  $f_{pN} = V_w / (6 \cdot 60 \cdot 60)$

$$K_g = \frac{P_{g0}}{T_{gN} - T_{zewN}} \quad K_1 = \frac{P_{gN} - c_{pp} \rho_p f_p (T_{zew} - T_{zew})}{T_{zewN} - T_{zewN}}$$

## Obiekty cieplne



Zakładamy, że  $T_g(t) = T_{gp}(t)$

$$\begin{cases} C_{vg} \dot{T}_{gp}(t) = c_{pw} \rho_{pw} f(t) T_{gz}(t) - c_{pw} \rho_{pw} f(t) T_{gp}(t) - K_g (T_{gp}(t) - T_{wew}(t)) \\ C_{vw} \dot{T}_{wew}(t) = K_g (T_{gp}(t) - T_{wew}(t)) - K_c (T_{wew}(t) - T_{zew}(t)) \end{cases}$$

$$\begin{cases} C_{vg} \dot{T}_{gp}(t) = c_{pw} \rho_{pw} f(t) (T_{gz}(t) - T_{gp}(t)) - K_g (T_{gp}(t) - T_{wew}(t)) \\ C_{vw} \dot{T}_{wew}(t) = K_g (T_{gp}(t) - T_{wew}(t)) - K_c (T_{wew}(t) - T_{zew}(t)) \end{cases}$$

wy:  $T_{gp}, T_{wew}$

we:  $T_{gz}, T_{zew}, f$

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$$\begin{cases} 0 = c_{pw} \rho_{pw} f (T_{gz} - T_{gp}) - K_g (T_{gp} - T_{wew}) \\ 0 = K_g (T_{gp} - T_{wew}) - K_c (T_{wew} - T_{zew}) \end{cases}$$

$$c_{pw} \rho_{pw} f (T_{gz} - T_{gp}) = K_g (T_{gp} - T_{wew}) = K_c (T_{wew} - T_{zew})$$

$$T_{wew} =$$

$$T_{gp} =$$

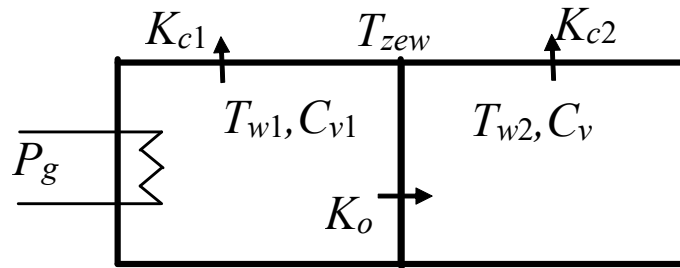
Identyfikacja parametrów ( $K_g, K_c$ )

1)  $T_{zewN}, T_{wewN}, T_{gzN}, T_{gpN}, f_N$

2)  $T_{zewN}, T_{wewN}, T_{gzN}, T_{gpN}, q_N$

$$c_{pw} \rho_{pw} f_N (T_{gzN} - T_{gpN}) = K_g (T_{gpN} - T_{wewN}) = K_c (T_{wewN} - T_{zewN}) = q_N$$

## Obiekty cieplne



$$\begin{cases} C_{v1} \dot{T}_{w1}(t) = P_g(t) - K_{c1}(T_{w1}(t) - T_{zew}(t)) - K_o(T_{w1}(t) - T_{w2}(t)) \\ C_{v2} \dot{T}_{w2}(t) = K_o(T_{w1}(t) - T_{w2}(t)) - K_{c2}(T_{w2}(t) - T_{zew}(t)) \end{cases}$$

wy:  $T_{w1}, T_{w2}$

we:  $P_g, T_{zew}$

$$\begin{cases} 0 = P_g - K_{c1}(T_{w1} - T_{zew}) - K_o(T_{w1} - T_{w2}) \\ 0 = K_o(T_{w1} - T_{w2}) - K_{c2}(T_{w2} - T_{zew}) \end{cases}$$

$T_{w1} =$

$T_{w2} =$

Identyfikacja parametrów ( $K_o, K_{c1}, K_{c2}$ )

Dane:  $P_{gN}, T_{zewN}, T_{w1N}, T_{w2}$

- 1) Konstrukcja zewnętrznych ścian jest taka sama, ale pomieszczenie 2 ma o połowę mniejszą powierzchnię ścian

$$K_{c2} = aK_{c1}, a = 0.5$$

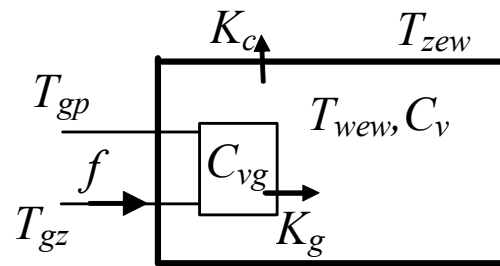
- 2) W warunkach nominalnych pomieszczenie z grzejnikiem 60% dostarczonego ciepła traci na zewnątrz

$$\left. \begin{array}{l} P_g \quad \text{dostarczane ciepło} \\ K_{c1}(T_{w1} - T_{zew}) \quad \text{strata na zewnątrz} \\ K_o(T_{w1} - T_{w2}) \quad \text{strata do pomieszczenia2} \end{array} \right\} \begin{cases} K_{c1}(T_{w1} - T_{zew}) = 0.6 \cdot P_g \\ K_o(T_{w1} - T_{w2}) = 0.4 \cdot P_g \end{cases}$$

$$K = \frac{kA_w}{a_g}$$

$K$  - w.jednostkowy, W/(mK)  
 $A_w$  - powierzchnia, m<sup>2</sup>  
 $a_g$  - grubość, m

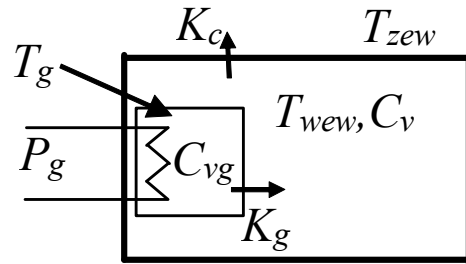




$$\begin{cases} C_{vg} \dot{T}_{gp}(t) = c_{pw} \rho_{pw} f(t) T_{gz}(t) - c_{pw} \rho_{pw} f(t) T_{gp}(t) - K_g (T_{gp}(t) - T_{wew}(t)) \\ C_{vw} \dot{T}_{wew}(t) = K_g (T_{gp}(t) - T_{wew}(t)) - K_c (T_{wew}(t) - T_{zew}(t)) \end{cases}$$

$$\begin{cases} C_{vg} \dot{T}_{gp}(t) = c_{pw} \rho_{pw} f(t) (T_{gz}(t) - T_{gp}(t)) - K_g (T_{gp}(t) - T_{wew}(t)) \\ C_{vw} \dot{T}_{wew}(t) = K_g (T_{gp}(t) - T_{wew}(t)) - K_c (T_{wew}(t) - T_{zew}(t)) \end{cases}$$

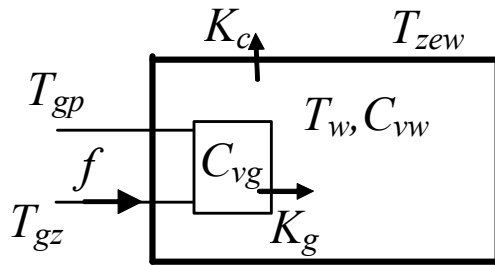
## Obiekty cieplne



$$\begin{cases} C_{vg} \dot{T}_{gp}(t) = P_g(t) - K_g (T_g(t) - T_{wew}(t)) \\ C_{vw} \dot{T}_{wew}(t) = K_g (T_g(t) - T_{wew}(t)) - K_c (T_{wew}(t) - T_{zew}(t)) \end{cases}$$

$$T_{wew}(s) = \frac{1}{M} q_g(s) + \frac{1}{M} T_{zew}(s)$$

$$T_g(s) = \frac{1}{M} q_g(s) + \frac{1}{M} T_{zew}(s)$$

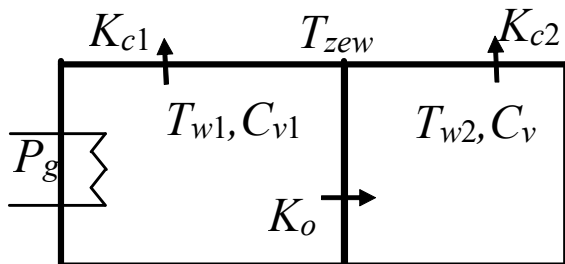


$$\begin{cases} C_{vg} \dot{T}_{gp}(t) = c_{pw} \rho_{pw} f(t) (T_{gz}(t) - T_{gp}(t)) - K_g (T_{gp}(t) - T_{wew}(t)) \\ C_{vw} \dot{T}_{wew}(t) = K_g (T_{gp}(t) - T_{wew}(t)) - K_c (T_{wew}(t) - T_{zew}(t)) \end{cases}$$

$$f(t) = const$$

$$T_{wew}(s) = \frac{1}{M} T_{gz}(s) + \frac{1}{M} T_{zew}(s)$$

$$T_{gp}(s) = \frac{1}{M} T_{gz}(s) + \frac{1}{M} T_{zew}(s)$$



$$\begin{cases} C_{v1} \dot{T}_{w1}(t) = q_g(t) - K_{c1} (T_{w1}(t) - T_{zew}(t)) - K_o (T_{w1}(t) - T_{w2}(t)) \\ C_{v2} \dot{T}_{w2}(t) = K_o (T_{w1}(t) - T_{w2}(t)) - K_{c2} (T_{w2}(t) - T_{zew}(t)) \end{cases}$$